

2.4. Fracture resistance for full saturation with one or other solution

fracture resistance R_s and R_d are defined as the ratio of the fracture resistance to the total resistance R (Table 1). The fracture resistance R_s is defined as the ratio of the fracture resistance to the total resistance R (Table 1). The fracture resistance R_d is defined as the ratio of the fracture resistance to the total resistance R (Table 1).

$$\frac{R_s}{R_d} = \frac{\rho_s}{\rho_d} = 0.82 \pm 0.02. \quad (1)$$

The fracture resistance R_s is defined as the ratio of the fracture resistance to the total resistance R (Table 1). The fracture resistance R_d is defined as the ratio of the fracture resistance to the total resistance R (Table 1).

$$\frac{R_{channel}}{R_{barrier}} = 0.85 \pm 0.03. \quad (2)$$

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$$R^* = \frac{R - R_d}{R_s - R_d}, \quad (3)$$

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Table 1
 $R_s, R_d, R_d/R_d$: Fracture resistance R_s and R_d are defined as the ratio of the fracture resistance to the total resistance R (Table 1). The fracture resistance R_s is defined as the ratio of the fracture resistance to the total resistance R (Table 1). The fracture resistance R_d is defined as the ratio of the fracture resistance to the total resistance R (Table 1).

	R_s (kΩ)	R_d (kΩ)	R_s/R_d	R/R^{pp}
Barrier	25.5	30.5	0.83	0.01
Channel	21.5	26.5	0.81	0.01

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3. Displacement experiments: results

3.1. Channel geometry

The fracture resistance R_s is defined as the ratio of the fracture resistance to the total resistance R (Table 1). The fracture resistance R_d is defined as the ratio of the fracture resistance to the total resistance R (Table 1).

3.2. Barrier geometry

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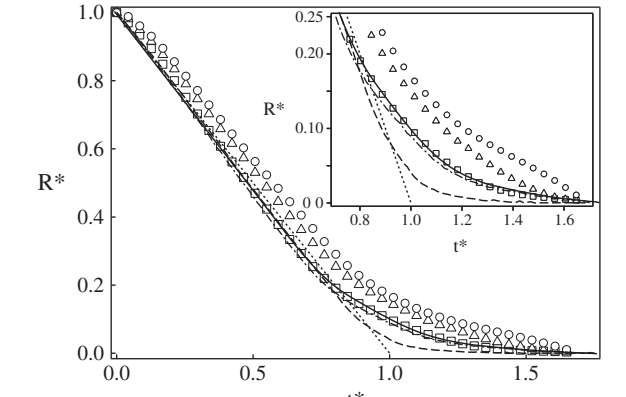


Fig. 4. Variation of the normalized fracture resistance R^* (Eq. (3)) versus normalized time $t^* = Ut/L$ for different Péclet numbers Pe : (○): $Pe = 28$, (△): $Pe = 142$, (□): $Pe = 285$. The inset shows a magnified view of the region where $t^* > 0.8$ and $R^* < 0.25$. The data points are fitted with a model where $n = 1$ and $n = 4.2$.

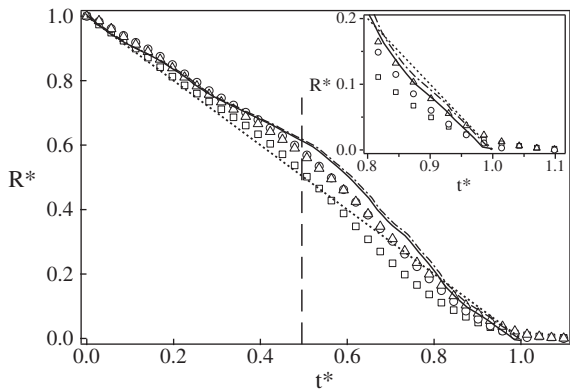


Fig. 5. Variation of R^* versus t^* for $Pe = 285$. The solid line represents the theoretical solution (Eq. (10)), and the symbols represent experimental data. The inset shows a zoomed-in view of the region where t^* is between 0.8 and 1.1 and R^* is between 0.0 and 0.2.

4. Displacement experiments: models

4.1. Parallel plates geometry

The flow in a parallel plate geometry is characterized by the Péclet number $Pe = Ut/a$, where U is the average velocity, t is the time, and a is the half-width of the channel. The dimensionless time t^* is defined as $t^* = Ut/L$, where L is the length of the channel. The dimensionless concentration c_d is defined as $c_d = (c - c_0)/(c_1 - c_0)$, where c is the concentration, c_0 is the initial concentration, and c_1 is the concentration at the inlet. The dimensionless retention factor R^* is defined as $R^* = R/R_0$, where R is the retention factor and R_0 is the retention factor at $t^* = 0$.

The concentration profile $c_d(\zeta)$ is given by (Boschan et al., 2003; Taylor, 1953):

$$c_d(\zeta) = \frac{1}{2}(1 \pm \text{Erf}(\zeta)); \quad (5)$$

where $\zeta = (x - Ut)/(2\sqrt{Dt})$, x is the axial distance, U is the average velocity, D is the diffusion coefficient, and t is the time. The dimensionless concentration c_d is a function of ζ and t^* . The dimensionless retention factor R^* is a function of t^* and is given by (Eq. (10)).

The dimensionless retention factor R^* is defined as $R^* = R/R_0$, where R is the retention factor and R_0 is the retention factor at $t^* = 0$.

$$R(t) = \frac{1}{aw} \int_0^L \rho(x, t) dx, \quad (6)$$

where $\rho(x, y, t) = \rho(x, t)$ is the concentration profile, a is the half-width of the channel, w is the width of the channel, and L is the length of the channel. The dimensionless concentration c_d is defined as $c_d = (c - c_0)/(c_1 - c_0)$, where c is the concentration, c_0 is the initial concentration, and c_1 is the concentration at the inlet. The dimensionless retention factor R^* is defined as $R^* = R/R_0$, where R is the retention factor and R_0 is the retention factor at $t^* = 0$.

$$R(t) = \frac{1}{\sigma_s aw} \int_0^L \frac{1}{1 - \chi c_d(x, t)} dx, \quad (7)$$

where $\chi = 1 - \sigma_d/\sigma_s$, σ_d is the dispersion coefficient, and σ_s is the sorption coefficient. The dimensionless concentration c_d is defined as $c_d = (c - c_0)/(c_1 - c_0)$, where c is the concentration, c_0 is the initial concentration, and c_1 is the concentration at the inlet. The dimensionless retention factor R^* is defined as $R^* = R/R_0$, where R is the retention factor and R_0 is the retention factor at $t^* = 0$.

$$R(t) \approx \frac{1}{\sigma_s aw} \left(L + \chi \int_0^L c_d(x, t) dx \right). \quad (8)$$

The dimensionless concentration c_d is a function of ζ and t^* . The dimensionless retention factor R^* is a function of t^* and is given by (Eq. (9)).

$$R(t) \approx \frac{1}{\sigma_s w} \left(\frac{L}{a} + \chi \frac{Q}{a^2 w} t \right). \quad (9)$$

The dimensionless concentration c_d is a function of ζ and t^* . The dimensionless retention factor R^* is a function of t^* and is given by (Eq. (10)).

$$R^* = 1 - t^*. \quad (10)$$

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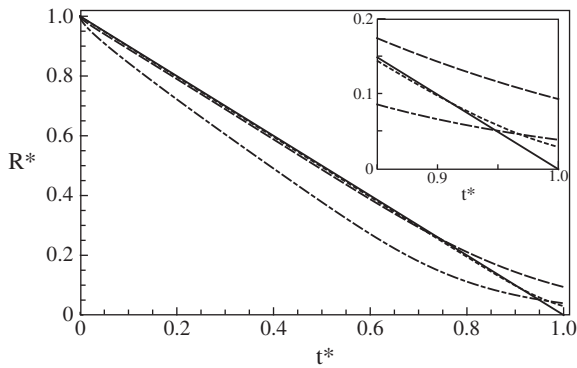


Fig. 6. The relationship between R^* and t^* for different values of α/a and χ . The curves correspond to $\alpha/a = 1$ (solid line), $\alpha/a = 10$ (dashed line), and $\alpha/a = 10$ (dotted line). The values of χ are $\chi = 0.12$ (solid line), $\chi = 0.7$ (dashed line), and $\chi = 0.7$ (dotted line).

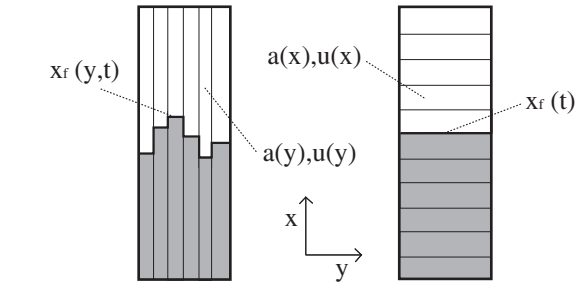


Fig. 7. Schematic diagram of the channel cross-section showing the velocity profile $u(x, y)$ and the concentration profile $a(x, y)$. The channel width is denoted by $x_f(y, t)$.

The velocity profile is assumed to be of the form $u(y) = \frac{\bar{u}a(y)^{(n+1)/n}}{\langle a(y)^{(n+1)/n} \rangle_y}$, where \bar{u} is the average velocity and $\langle a(y)^{(n+1)/n} \rangle_y$ is the average of $a(y)^{(n+1)/n}$ over the channel width. The concentration profile is assumed to be of the form $a(x, y) = a(y) \exp(-\mu x)$, where μ is a decay constant and $a(y)$ is the concentration at the channel entrance.

$$u(y) = \frac{\bar{u}a(y)^{(n+1)/n}}{\langle a(y)^{(n+1)/n} \rangle_y} \quad (11)$$

The average velocity \bar{u} is defined as $\bar{u} = \langle u(y) \rangle_y$, where $\langle \cdot \rangle_y$ denotes the average over the channel width. The concentration profile $a(x, y)$ is assumed to be of the form $a(x, y) = a(y) \exp(-\mu x)$.

$$x_f(y, t) = u(y)t \quad (12)$$

The channel width $x_f(y, t)$ is assumed to be proportional to the velocity $u(y)$. The concentration profile $a(x, y)$ is assumed to be of the form $a(x, y) = a(y) \exp(-\mu x)$, where μ is a decay constant and $a(y)$ is the concentration at the channel entrance.

4.2.2. Analytical computation of the resistance

The resistance R is defined as the ratio of the average velocity \bar{u} to the average concentration $\langle a \rangle$. The average velocity \bar{u} is defined as $\bar{u} = \langle u(y) \rangle_y$, where $\langle \cdot \rangle_y$ denotes the average over the channel width. The average concentration $\langle a \rangle$ is defined as $\langle a \rangle = \langle a(y) \rangle_y$, where $\langle \cdot \rangle_y$ denotes the average over the channel width.

$$\frac{1}{R(t)} = \frac{\sigma_s}{L} \int_0^w a(y) \left(1 - \frac{\chi}{L} \int_0^L c_d(x, y, t) dx \right) dy \quad (13)$$

The concentration profile $c_d(x, y, t)$ is assumed to be of the form $c_d(x, y, t) = a(y) \exp(-\mu x) \exp(-\lambda t)$, where μ is a decay constant, λ is a decay constant, and $a(y)$ is the concentration at the channel entrance.

4.2. Channel geometry

4.2.1. Velocity field and front displacement

The velocity field $u(x, y, t)$ is assumed to be of the form $u(x, y, t) = u(y) \exp(-\mu x) \exp(-\lambda t)$, where μ is a decay constant, λ is a decay constant, and $u(y)$ is the velocity at the channel entrance. The front displacement $x_f(y, t)$ is assumed to be proportional to the velocity $u(y)$.

$\frac{1}{R(t)} = \frac{\sigma_s}{L} \int_{u(y)t \leq L} a(y) \left(1 - \frac{\chi}{L} u(y)t\right) dy + \frac{\sigma_s}{L} \int_{u(y)t \geq L} a(y) (1 - \chi) dy$

$$\frac{1}{R(t)} = \frac{\sigma_s}{L} \int_0^w a(y) dy - \frac{\sigma_s \chi t}{L^2} \int_0^w a(y) u(y) dy \quad (14)$$

$U_M \leq 1$ (Eq. (14))

$$\frac{1}{R(t)} = \frac{\sigma_s}{L} \int_0^w a(y) dy - \frac{\sigma_s \chi t}{L^2} \int_0^w a(y) u(y) dy \quad (15)$$

$U_M \geq 1$ (Eq. (9))

$$R(t) = \frac{L}{\sigma_s \int_0^w a(y) dy} \left[1 + \frac{\chi t}{L} \int_0^w a(y) u(y) dy \right] \quad (16)$$

Eq. (10)

$t_1 = L/U_M$

$n = 0.26$

$Pe = 285$

$n = 1$

$n = 0.26$

Pe

4.2.3. Numerical 2D computation of the resistance

$2D$

$r(x,y)$

$$r(x,y) = \frac{\delta l}{\sigma a(x,y) \delta w} \quad (17)$$

$R^*(t^*)$

Pe

$R^*(t^*)$

Fl

4.3. Barrier geometry

4.3.1. Velocity field and front displacement

$dx_f/dt = u(x)$

$$t = \int_0^{x_f} \frac{dx}{u(x)} = \frac{w}{Q} \int_0^{x_f} a(x) dx \quad (18)$$

Fl

4.3.2. Analytical and numerical computation of the resistance

Q

$$R(t) = \frac{1}{\sigma_s w} \left(\int_0^L \frac{dx}{a(x)} + \chi \int_0^{x_f(t)} \frac{dx}{a(x)} \right) \quad (19)$$

dR/dt

$$\frac{dR(t)}{dt} = \frac{\chi}{\sigma_s w^2} \frac{Q}{a^2(x_f(t))} \quad (20)$$

$Q = a(x_f(t)) w dx_f/dt$

